A novel and sustainable approach to enhance the Li-ion storage capability of recycled graphite anode from spent lithium-ion batteries

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Abstract

The ubiquitous manufacturing of lithium-ion batteries (LIBs) on high consumer demand produces inevitable e-waste that imposes severe environmental and resource sustainability challenges. In this work, the charge storage capability and Li-ion kinetics of recovered water-leached graphite (WG) anode from spent LIBs is enhanced by using an optimized amount of recycled graphene nanoflakes (GNF) as an additive. WG@GNF anode exhibits an initial discharge capacity of 400 mAh g\(^{-1}\) at 0.5C with 88.5% capacity retention over 300 cycles. Besides, it delivers an average discharge capacity of 320 mAh g\(^{-1}\) at 500 mA g\(^{-1}\) over 1000 cycles, which is 1.5-2 times higher than WG. The sharp increase in electrochemical performance is due to the synergistic effects of Li-ion intercalation into the graphite layers and Li-ion adsorption into the surface functionalities of GNF. Density functional theory calculations reveal the role of functionalization behind the superior voltage profile of WG@GNF. Besides, the unique morphology of spherical graphite particle trapping into graphene nanoflakes provides mechanical stability over long-term cycling. This work explains an efficient strategy to upgrade the electrochemical compatibility of recovered graphite anode from spent LIBs towards next-generation high-energy-density LIBs.

Keywords: recycling, spent lithium-ion batteries, anode, graphite, graphene nanoflakes, electrochemistry, DFT calculation.
Introduction

The forefront of battery research in modern civilization aims towards high power and high energy density applications in scientific and industrial fields with reduced cost, improved safety, cycle-life, and superior rate capability. Over the past few decades, lithium-ion batteries (LIBs) have become a leading technology in the emerging sectors of portable electronic and electric vehicles (EVs) appliances.\(^1^,\(^2\) However, the vast manufacturing of LIBs and the generation of inevitable e-waste after their lifespan have raised significant concerns in economic and environmental prospects.\(^3\) The global LIB market value is anticipated to reach $139 billion by 2029 to fulfil the ever-growing consumer demand.\(^4\) It may produce over 11 million tons of discarded LIBs between 2017 and 2030.\(^5\) This upsurges the need for developing novel recycling strategies for the spent LIB components.

Graphite is a state-of-art commercialized anode material due to its low lithiation potential (<100 mV), high conductivity, and high electrochemical stability (>1000 cycles). The government of the United States of America and Europe have classified graphite as a critical mineral for increasing the demand by 10-12% every year.\(^6\) To date, the price of graphite has become $20/kg.\(^7\) The market value of graphite is forecasted to hit $21.6 billion by 2027 with a CAGR of 5.3%.\(^8\) Current LIB recycling strategies mainly focus on cathode recovery for valuable metals (Li, Co etc.).\(^9^,\(^10\) In the pyrometallurgy process, the carbon anode is burnt in a smelter furnace to recover the cathode by carbo-thermal reduction. During this process, the carbon anode is oxidized into CO\(_2\) (a poisonous gas) and Li\(_2\)CO\(_3\) (as slag); thus, graphite cannot be recovered.\(^11\) Whereas in hydrometallurgy, carbon is settled down during solvent extraction and separation. The recovered carbon by this method is of poor quality and needs high production costs for battery-grade
applications. In comparison, the physical dismantling process is effective for graphite recovery, though this process is challenging for scaling up to the industry level.

However, the theoretical capacity of graphite is limited to 372 mAh g\(^{-1}\) (corresponding to the LiC\(_6\) phase), and it impedes to compete with the ongoing energy crisis. Besides insertion-type anodes, alloy and conversion-type materials (theoretical capacity of \(\sim1000\) mAh g\(^{-1}\))\(^{13,14}\), various advanced carbonaceous materials like graphene, carbon nanotube (CNT), carbon nanofiber (CNF), hard carbon, etc., have been studied extensively to reveal Li-ion storage properties. Among them, 2D nanostructured graphene stole the limelight as LIB anode due to incredible electronic transport phenomena, flexibility, conductivity, wide electrochemical window, and more Li-ion storage capability.\(^{15}\) This results in a high capacity of 744 mAh g\(^{-1}\), 780 mAh g\(^{-1}\), and 1114 mAh g\(^{-1}\) for the formation of LiC\(_3\), Li\(_2\)C\(_6\), or LiC\(_2\), respectively, depending on Li\(^+\) intercalation and adsorption in both sides and edges of graphene sheets.\(^{16,17}\) However, literature reports the limited cyclability of graphene anode alone within hundreds of cycles with \(\sim50\)% capacity loss due to irreversible Li\(^+\) trapping and aggregation of graphene sheets, although it delivers high capacity during the initial cycle. Besides, large-scale synthesis of graphene due to very low-density material and high irreversible capacity loss (>50%) restricts the commercialization of graphene batteries. Meanwhile, compositing graphene with carbonaceous materials (e.g., carbon nanofiber, CNT, graphite foil, etc.) can enhance electrochemical performance as illustrated in Supporting Information Table S1 in terms of charge-discharge cycling stability and capacity retention with respect to the cycle number in comparison to our study with recycled graphite material.\(^{18}\)\(^{19–22}\)

Generally, the degradation of graphite anode on prolonged cycling is attributed to the formation of a thick solid electrolyte interface (SEI) layer on the graphite surface due to the reductive decomposition of electrolyte solvents and salt anions.\(^{23,24}\) The SEI layer and solvated
Li-ion create pressure that results in the cracking and splitting of graphite flakes. The damaged, exposed surfaces are prone to further surface reactions, which deteriorate the cell performance. In a cycled graphite, the layers can expand up to 10.3%.\textsuperscript{18} The bulk structural integrity and crystal lattice of the graphitic matrix is still retained. Therefore, after some post-purifications, the recovered graphite can be reused as anode material for LIBs. In reported literature, the black mass recovery and electrochemical activity of electrode materials are restored by acid leaching (H\textsubscript{2}SO\textsubscript{4}-H\textsubscript{2}O\textsubscript{2}, HCl-H\textsubscript{2}O\textsubscript{2}, organic acids, etc.), NMP or microwave-assisted deep eutectic solvents based leaching.\textsuperscript{4,25–27,27–34} Herein, we focus on improvising the electrochemical performance of water-leached recovered graphite by using a conductive additive to the recovered graphite matrix instead of any acidic solvent washing, as reported earlier.

A recent publication from our group observed that graphite is recovered from spent laptop battery packs by facile water leaching method\textsuperscript{35} and further calcined under an inert atmosphere at 750 °C to eliminate residual impurities and improve the degree of graphitization of the recovered graphite. Recovered water-washed graphite (WG) delivered a stable discharge capacity of 310 mAh g\textsuperscript{-1} at 0.1 C rate over 100 cycles and 295 mAh g\textsuperscript{-1} at 0.5 C rate over 1000 cycles, respectively.\textsuperscript{36} Herein, the specific capacity of WG is further improvised by compositing with graphene nanoflakes (GNF) as a conductive additive synthesized from WG by modified Hummer’s method. Electrochemistry reveals that optimized WG@GNF displays superior C-rate performance and an average discharge capacity of 320 mAh g\textsuperscript{-1} with 62 % capacity retention over 1000 cycles (156 mAh g\textsuperscript{-1} for WG) at a higher current density of 500 mA g\textsuperscript{-1}. Experimental characterizations coupled with DFT calculations reveal that the higher reversible Li-ion storage with the voltage profile is attributed to the synergistic phenomena of Li-ion intercalation and adsorption into the tailored surface functionalized WG@GNF. To check the potential feasibility of WG@GNF as the
anode, full cells are fabricated with commercial NMC 811 and LFP cathodes. This study reveals the comprehensive utilization of graphite anode from spent LIBs and improvements in its specific capacity through precise compositing with graphene nanoflakes, which pave the way for a promising active anode material for high-performance Li-ion batteries.

**Experimental methods**

**Graphite recovery from spent LIBs and post-purification** Spent lithium-ion laptop batteries were provided by Nile Limited, Hyderabad, India. 18650 type cylindrical cells were discharged first by short-circuit method below 2V for safety issues. The cells were then manually dismantled, and the anode part was carefully segregated from the Swiss roll assembly of the electrode separator. The anode black mass is recovered from the copper foil current collector by water leaching. The binder dissolves, separating the anode black mass from the copper foil current collector. This process eliminates surface-adsorbed lithium and lithium-containing SEI components (e.g., Li$_2$O, Li-alkyl carbonates, bicarbonates, Li$_2$CO$_3$, etc.) from the graphite surface by H$_2$ evolution reaction. The anode black mass is filtered and dried at 90°C overnight. It is then calcined at 750 °C for 5 hours under an argon atmosphere to eliminate carbon black additives, Li-salts, and electrolyte-decomposed impurities from the graphite surface. This purified graphite is termed water-washed graphite (WG).

**Synthesis of graphene nanoflakes (GNF) from recycled graphite**

GNF is synthesized from WG by modified Hummer’s method. First, 1g of WG is added to 1g NaNO$_3$ in 46 ml concentrated H$_2$SO$_4$ medium and stirred in an ice bath for 4 hours. Next, 6g of KMnO$_4$ is added and stirred at 35°C for 2 hours. After that, 92 ml of ice-cold DI-water is added and refluxed at 98°C for 2 hours. Finally, 50 % H$_2$O$_2$ is added and repeatedly washed with 1:3 HCl:
water mixture and DI water until a neutral pH is obtained. The resultant graphene oxide (GO) is dried overnight at 70°C. It is then calcined at 500°C for 30 mins under an inert atmosphere and reduced thermally to graphene nanoflakes (GNF).

**Regeneration of recovered water-washed graphite**

An optimized weight ratio of 20 wt.% of recycled GNF is mixed with recovered water-washed graphite (WG) in DI-water solvent, ultrasonicated for 15 mins at room temperature, and dried overnight at 70°C. Here, GNF is used as an additive to the graphite matrix, and the regenerated material is termed WG@GNF. Scheme 1 describes the flowchart of the overall regenerating process of anode graphite.

![Scheme 1. Flowchart of the overall regenerating process of graphite anode.](image-url)
**Structural and Morphological Characterizations.**

The powder XRD was analyzed by X’Pert Pro diffractometer (The Netherlands) using Cu Kα radiation (λ = 1.54 Å), reflection θ−θ geometry, receiving slit of 0.2 mm, scintillation counter, 30 mA, and 40 kV. The diffraction data were collected between the 2θ angle of 5-80°. Raman spectroscopy was conducted using a micro-Raman spectrometer HR800 (Jobin Yvon Horiba, France), with He-Ne laser of excitation line 632.8 nm and a microscope objective (50X, Olympus MPlan, 0.4 mm working, numerical aperture 0.75 in backscattering configuration). The surface morphologies were carried out by scanning electron microscopy (JEOL-FESEM). FTIR spectroscopy was carried out in Bruker Alpha-P FTIR spectrometer. XPS was measured using ESCA+ (Omicron Nanotechnology, Oxford Instruments Plc., Germany) equipped with monochromic AlKα (1486.6 eV) X-ray beam radiation operated at 15 kV, 20 mA. The binding energy was calibrated vs. carbon (C 1s = 284.6 eV).

**Cell Assembly and Electrochemical Characterizations.**

The electrochemical performances were carried out in CR2032-type coin cells. The slurry composition was 90 wt.% of the graphite-based anode active material and 10 wt.% PVDF binder (Kureha 1700) in NMP solvent. The slurry was coated onto a copper foil current collector using a doctor blade. Electrodes were dried overnight at 80°C under vacuum and calendared, followed by punching into a circular disc of 10 mm diameter. The active material loading was 1.2± 0.3 mg cm⁻². The coin cells were fabricated inside the glove box (mBraun, Germany) with O₂ and H₂O levels less than 0.1 ppm. Pure-Li metal chip was used as a reference and counter electrode half-cell study, and the electrolyte is 1M LiPF₆ in ethylene carbonate-diethyl carbonate solvent. The electrochemical analysis, such as charge-discharge cycling and C-rate performance at different current densities for the electrode, was carried out using Arbin battery testing instruments (Arbin
BT2000-Battery test equipment). Cyclic voltammetry and impedance studies were performed in the cell test system model 1470E coupled with an FRA model 1455A (Solartron Analytical Oak Ridge, TN) instruments.

**Computational Details**

First-principles calculations based on density functional theory (DFT) are carried out as implemented in the PWSCF Quantum-Espresso package.\(^{39}\) Geometry optimization, including dispersion correction,\(^{40}\) was performed using GGA-PBE\(^ {41}\) level of theory, and the electrons-ions interactions were described by ultrasoft pseudo-potentials with electrons from C 2s, 2p; O 2s, 2p; Li 2s; shells explicitly included in calculations. Plane-wave basis set cutoffs for the smooth part of the wave functions, and the augmented density was 25 and 200 Ry, respectively. Both ions and volume were relaxed during the optimization of the bulk structures. Geometry optimizations for 6 × 6 × 2 supercell were performed with a k-point\(^ {42}\) sampling of 3 × 3 × 3 for both graphite and composite models. Composite models have been constructed by functionalizing one layer of bulk 6 × 6 × 2 supercell graphite with oxygen atoms (explained in detail in Supporting Information Text S1 and Figure S1).

The binding energy of the Li atom has been calculated using the following relation

\[
E_{\text{Binding}} = E_{C_{288}Li_x} - E_{C_{288}} - xE_{Li}
\]

Where \(E_{C_{288}Li_x}\) is the energy of the bulk Li atoms intercalated graphite, \(xE_{Li}\) is the energy of the Li atoms and \(E_{C_{288}}\) is the energy of the bulk graphite. The average voltage (V) during the Li intercalation process \((Li + C_{288} \rightarrow Li_x C_{288};\) where \(x\) is the number of Li intercalated into graphite\) can be written in the form of the change in Gibbs free energy \((\Delta G_f)\)\(^ {43-46}\)
\[ V = - \frac{\Delta G_f}{zF} \]

Where \( z \) and \( F \) are the number of valence electrons during the intercalation process and the Faraday constant, respectively; \( \Delta G_f \) is the change in Gibbs free energy during the intercalation process, which is defined as

\[ \Delta G_f = \Delta E + P \Delta V - T \Delta S \]

\( P \Delta V \) is on the order of \( 10^{-5} \) eV, and the term \( T \Delta S \) is comparable to 26 meV at room temperature; thus, the entropy and pressure terms are negligible.\(^{43,44,46} \) \( \Delta G_f \) is then approximately equal to the total energy change (\( \Delta E \)) involved in the system, which is defined as

\[ \Delta E = E_{Li_xC_{288}} - E_{Li_x} - E_{C_{288}} \]

where \( E_{Li_xC_{288}} \) is the total energy of the Li intercalated graphite system, \( E_{Li_x} \) is the energy of intercalated Li-atoms and, \( E_{C_{288}} \) is the energy of the pristine graphite system, respectively.

Therefore, the voltage is given by the equation

\[ V = - \frac{E_{Li_xC_{288}} - E_{Li_x} - E_{C_{288}}}{zx} \]

Similarly, for the composite system, the voltage is calculated by the following equation,

\[ V = - \frac{E_{Li_xC_{288}O_{12}} - E_{Li_x} - E_{C_{288}O_{12}}}{zx} \]

Specific capacity has been calculated using the following equation,\(^{47,48} \)

\[ C = \frac{nxF}{M_f} \]
Where \( n \) is the number of electrons transferred per formula unit, \( x \) is the number of Li atoms intercalated, \( F \) is the Faraday constant, and \( M_f \) is the mass of the formula unit. Charge difference distribution (CDD) has been obtained using the equation,\(^{49,50}\)

\[
\rho_{\text{CDD}} = \rho_{\text{Total}} - \sum_i \rho_{i}^{\text{Fragment}}
\]

where, \( \rho_{\text{Total}} \) is the total charge density of the system, and \( \rho_{i}^{\text{Fragment}} \) represents the charge density of the individual fragments.

**Results and discussions**

**Morphological and structural characterizations.**

SEM analysis is conducted to understand the morphological characteristics of pristine recovered and reformed graphite. Figure 1a represents water-washed recovered graphite with the agglomeration of graphite particles having secondary impurities on the surface of the graphite particles. However, the roughness of the graphite surface is diminished, and the electrolyte decomposed products are eliminated on thermal treatment, as shown in Figure 1b. Further, to understand the effect of washing upon impurity removal, we have conducted the elemental mapping analysis of scrapped graphite (without washing) and the purified graphite. The elemental mapping of scraped graphite (Supporting Information Figure S2a) shows the presence of O, F, P elements in addition to C due to SCMC binder, LiPF\(_6\) salt and electrolyte decomposed products. After purification, O, F, and P elements reduce in WG, showing the strong presence of C (Supporting Information Figure S2b). Besides, spherical graphite particles are trapped in the wrinkled graphene flakes,\(^{19}\) as shown in the surface microstructure of WG@GNF in Figure 1c. Figure 1d is the magnified image of Figure 1c that represents with flocculent morphology of wrinkled graphene nanoflakes. Similarly, Figure 1e is the magnified image of Figure 1c, where
the smooth surface and graphite flakes are visible. EDS mapping of WG@GNF (Supporting Information Figure S2c) further confirms the uniform distribution of elemental O in the carbon matrix, and the atomic % of carbon and oxygen are 84.4 % and 15.6 %, respectively. Besides, TEM images also validate similar morphologies. Figures 1f-g show the overall particle and edge view of WG@GNF, indicating that the spherical graphite particle is encapsulated within thin graphene layers. Figure 1 h-i is the magnified boundary image with clear visibility of the ordered layered arrangement of graphite layers and randomly oriented graphene sheets of WG@GNF. This unique morphology might facilitate the infiltration of electrode material and reduce the agglomeration of graphene flakes that might provide structural integrity during the electrochemical charge-discharge cycling process. Supporting Information Figures S3a-S3b represent the TEM images of as-synthesized recycled graphite (WG) and recycled graphene nanoflakes (GNF), respectively.
Figure 1. Scanning electron microscopy images of (a) recovered water-washed graphite, (b) water-washed graphite purified by heating under inert condition (WG), (c) WG@GNF, zoomed image of (d) GNF portion, (e) WG portion and transmission electron microscopy images of (f-i) WG@GNF.

The XRD pattern of WG@GNF in Figure 2a is compared with pristine recycled graphite WG. The appearance of a sharp peak at $2\theta = 26.5^\circ$ for the (002) plane (JCPDS# 00-056-0159) confirms that the hexagonal crystal system is retained in the recovered graphite. However, the peak broadens in WG@GNF and shifts to a lower $2\theta$ angle for disordered graphene sheets. The interplanar spacing ($d_{002}$) is increased from 3.35Å for WG to 3.37Å for WG@GNF. The peak at 42.3° for the (100) plane and 44.5° for the (101) plane arises due to the hexagonal phase of exfoliated graphite sheets in WG@GNF, which are insignificant in WG (Figure 2b). However, these peaks are more widened in bare recycled GNF, as shown in Supporting Information Figure S4, with an enlarged interplanar spacing $d_{002}$ of 3.65 Å. $d_{002}$ is calculated based on Bragg’s equation ($2d \sin \theta = n \lambda$).

We have simulated the X-ray diffraction pattern of the DFT-optimized WG and WG@GNF systems (Supporting Information Figure S5). As seen from Figure 2b, the $2\theta$ value is less in WG@GNF, which matches the trend of the experiment. However, the relative change of $2\theta$ between WG and WG@GNF is more in theory (differs by $2\theta$ of 1.1) than in the experiment (varies by $2\theta$ of 0.2). The difference might be due to the consideration of a single functionalized graphite layer in the simulation model, whereas in experiment, the functionalized layers are composed of nanoflakes morphology, thus expecting a more packed nature of the functionalized layers. Nevertheless, the less $2\theta$ value in composite structures represents the increase in lattice volume compared to graphite structures. This is similar to the experimental trend in which an increased lattice volume was observed due to functionalization.
Figure 2. (a) X-ray diffraction patterns, (b) simulated XRD (inset: peak position of (002) plane in the experimental), (c) Raman spectra of WG@GNF and WG; (d) FTIR spectra, and (e) XPS plots of WG@GNF for C1s and O1s.

Raman spectroscopy (Figure 2c) is carried out for WG@GNF and WG to understand the distinct structural features and vibrational modes in terms of defects and disorders in the graphitic lattice. The spectra display two strong peaks at 1350 and 1580 cm\(^{-1}\) originating from the G-band (attributed to in-plane stretching vibrations of sp\(^2\) carbons) and D-band (corresponding to disordered carbon at the edges and defect sites), respectively. The D-band (I\(_D\)) and G-band (I\(_G\)) ratios slightly increased from 0.4 for WG to 0.52 for WG@GNF. It indicates the presence of
disorderness arising from GNF due to the exfoliation of graphene layers, defect sites, and surface functionalities.

The nature of the functional groups present in WG@GNF is investigated by the Fourier transform infrared (FTIR) spectra (Figure 2d) analysis indicating the bonding nature and composition of the carbon matrix. The characteristic peak at 1630 cm\(^{-1}\) denotes in-plane vibration of C=C stretching from sp\(^2\) hybridized graphitic carbons. A peak at 1735 cm\(^{-1}\) might be from C=O groups of \(-\text{COOH}\). A broad peak \(~1000\text{ cm}^{-1}\) is related to C–O containing different functional groups originating from oxidized carbon at edges like alcohols, carboxyl, esters, etc. The peak at 3400 cm\(^{-1}\) arises from H-bonded \(-\text{OH}\) stretching.

X-ray photoelectron spectroscopy is conducted to validate further these functional groups' bonding, composition, and surface chemistry in WG@GNF, as represented in Figure 2e. The notable peaks in C1s spectra at 283.2, 284.8, 285.7, and 287.2 eV correspond to C-Li linkage (from Li intercalation compounds LiC\(_6\)), C-C (sp\(^2\) carbon), C-O (epoxide and hydroxyl groups) and C=O (alkyl carbonates), respectively. Besides, in O1s spectra, the peaks at \(~531.4, 532.9, \text{ and } 535\text{ eV}\) denote C-O, C=O, and O-C=O linkages. In addition, peaks at 529.1 and 530 eV arises due to Li\(_2\)O and Li\(_2\)CO\(_3\) inorganics from SEI components in cycled graphite. The surface chemistry affirms the presence of controlled oxygen functionalities in the graphite matrix that might directly influence the electrochemical performance of the regenerated graphite material from spent LIBs. Thus, it projects WG@GNF as a promising anode for high-performance LIBs.

**Electrochemical characterizations**

In a recent study, we observed that water-washed recycled graphite (WG) exhibits an average discharge capacity of 315 mAh g\(^{-1}\) at 0.1C. The capacity of graphite originates from Li-ion
intercalation into the layers and the formation of stable lithium intercalation compounds LiC₆, corresponding to the maximum theoretical capacity of 372 mAh g⁻¹. The site-controlled Li⁺ diffusivity of WG can be surmounted in graphene-based systems by introducing the optimum amount of oxygen and hydrogen-containing heteroatom functionalities. To understand the Li-storage behaviour of pristine recycled graphene nanoflakes (GNF) anode material in LIBs, galvanostatic charge-discharge analysis is carried out at a lower current density of 50 mA g⁻¹.

Figure 3a represents that recycled GNF delivers an initial discharge capacity of 1280 mAh g⁻¹ with 48% coulombic efficiency (CE). However, in 2nd cycle, capacity fades deeply to 50% with 658 mAh g⁻¹. Very high initial capacity is attributed to the surface adsorption of Li⁺ into pores and defect sites. The irreversibility arises due to the solid electrolyte interface (SEI) formation and trapping of Li⁺. Such high irreversible capacity during initial cycles is undesirable for practical applications of pure graphene anodes.¹⁵,⁵¹ However, the superior Li-storage capability of GNF can be utilized by using an optimized amount of GNF as an additive to recycled water-washed graphite (WG@GNF), minimizing the initial irreversibility. In other words, the capacity of WG will be further enhanced with more numbers of Li-ion accommodation sites by intercalation and adsorption phenomena simultaneously. Supporting Information Figure S6a-S6d represents the capacity vs. voltage profile of different compositions of GNF additive (such as 100%, 80%, 40% and 20%) to the recycled graphite matrix. Further, Supporting Information Table S2 signifies the irreversible capacity loss during discharge and charge in 1st cycle and irreversible discharge capacity in 2nd cycle. The coulombic efficiency in 1st cycle is observed to be improvised from 48% (for GNF) to 72% (for 20% GNF additive). Figure 3b shows that the optimized WG@GNF electrode delivers an initial discharge capacity of 800 mAh g⁻¹, and the irreversible capacity reduces to 26% in 2nd cycle (49 % for recycled GNF) under similar conditions. Thus, it is evident
that despite high irreversibility in graphene systems, its charge storage property can be used to enhance the capacity of recycled graphite anode for high-energy-density LIB applications.

**Figure 3.** Galvanostatic charge-discharge voltage profile of (a) recycled GNF and (b) WG@GNF at a lower current density of 50 mA g\(^{-1}\).

The lithiation (discharge) and delithiation (charge) behavior for WG@GNF and WG are evaluated by cyclic voltammetry study within the voltage window of 0.01–1.5 V and 0.01–3 V for WG and WG@GNF, GNF, respectively. Figures 4a and 4b represent the CV plots for WG and WG@GNF, respectively, at a scan rate of 0.05 mV s\(^{-1}\). The notable lithiation peaks below 100 mV indicate the formation of stable Li intercalation phases of LiC\(_{12}\) and LiC\(_{6}\) in both the anodes. An additional hump in WG@GNF at 0.67 V during 1\(^{st}\) lithiation process arises due to the passivating SEI film by reductive decomposition of the electrolyte. The absence of this peak during subsequent cycles indicates the formation of a stable SEI layer that enhances Li\(^+\) passivation to the graphitic surface. Besides, the expanded area of the CV curve around 3 V is attributed to the surface-induced Li\(^+\) adsorption process into edges and defect sites of the graphene flakes (Figure 4b). It concludes
on simultaneous happenings of surface adsorption of GNF and Li$^+$ intercalation into the graphite layers, which induces extra charge storage capability in WG@GNF. The larger area under the CV curve and higher peak current density signifies better Li-ion kinetics in WG@GNF. The CV curve for bare recycled GNF (Supporting Information Figure S7) shows a broad curve during lithiation and delithiation. No distinct peaks for Li intercalation compounds in recycled GNF indicate surface adsorption property, intercalation as LiC$_x$ nanopore filling. The observed charge storage property from CV plots is in good agreement with the galvanostatic charge-discharge voltage profile at the 0.1 C rate. Figure 4c exemplifies the cumulative profiles for WG@GNF and WG at 0.1 C rate, where the unique characteristics of charge storage behaviours can be clearly noticeable. WG@GNF shows adsorption-intercalation property (866 mAh g$^{-1}$ discharge capacity in 1$^{st}$ cycle). In comparison, WG exhibits only Li intercalation phenomena (394 mAh g$^{-1}$ discharge capacity in 1$^{st}$ cycle) below 0.2V. Figure 4d represents a histogram that quantifies the capacity contribution from the slopy region (surface adsorption phenomena >0.2V) and plateau region (intercalation phenomena <0.2V) voltage profiles of WG@GNF in comparison to WG at 0.1C. It signifies that the extra capacity originates from the slopy region surface adsorption of Li$^+$ into edges and defect sites of graphite sheets in WG@GNF, where the intercalation capacity contribution remains almost the same.
Figure 4. Cyclic voltammetry plots of (a) WG and (b) WG@GNF, (c) galvanostatic charge-discharge voltage profile of WG@GNF and WG at 0.1C rate, (d) the histogram quantifying the capacity contribution from surface adsorption >0.2V and intercalation <0.2V from (c).

To better understand the voltage profiles, DFT calculation has been performed for the staggering mechanism of Li-ion intercalation into the WG and WG@GNF system. This mechanism proceeds through different stages with a varying periodic repeat distance between two neighbouring Li-ion intercalant layers. A higher stage number (n) corresponds to a lower intercalant concentration and more empty graphene–graphene layers, implying a lower charge storage capacity. To simulate the staging mechanism, three different stages (stage-4, stage-
2 and stage-1) of intercalation are modelled as shown in Figure 5a, considering two different concentrations for stage-4 in both graphite and composite system. Stage-4 has also been modelled with lower Li-concentration, which is referred to as stage-4′ in the case of the graphite system. On the other hand, another model is stage-4″ which represents a quasi-stage-4′ Li intercalation, where the Li atoms are intercalated on both sides of the oxygen-functionalized layer. Therefore, considering the C₆[Li]ₓ formula unit, the x-values result in 0.125, 0.25, 0.5 and 1.0 for stage-4′, stage-4, stage-2 and stage-1, respectively, for graphite, whereas the x-values are 0.125, 0.25, 0.5 and 0.75 for stage-4′, stage-4″, stage-2 and stage-1, respectively for composite. Thus, the resulting specific capacity for stage-4′, stage-4, stage-2 and stage-1 of graphite are 46.5, 93.0, 186.0 and 372.1 mAh g⁻¹, respectively. Similarly, the resulting specific capacity for stage-4′, stage-4″, stage-2 and stage-1 of the composite are 44.1, 88.1, 176.2 and 264.5 mAh g⁻¹, respectively. As can be seen from Figure 5b, the voltage decreases with the increase of Li-ion intercalation for both WG and WG@GNF composite systems during the charging process. The calculated voltages for stage-4′, stage-4, stage-2 and stage-1 are 0.80, 0.35, 0.32, -0.14 V vs. Li⁺/Li, respectively for WG, whereas the calculated voltages for stage-4′, stage-4″, stage-2 and stage-1 are 2.60, 2.36, 1.27 and 0.74 V vs. Li⁺/Li, respectively for WG@GNF composite. Notably, the calculated voltage for stage-1 of graphite shows a negative value, which might be due to the consideration of dispersion correction in DFT to describe the Van-der Waal interaction accurately. Nevertheless, it is interesting to note that, for a similar range of capacity, the voltage is more in the case of the WG@GNF compared to WG. Also, voltage is higher in WG@GNF composite than graphite across the studied capacity range, thus matching nicely with the experimental trend. In fact, the voltage of the first intercalation step for each stage is significantly higher than that of the other succeeding intercalation steps, which is in agreement with the experimental result. The reason is expected to
be that widening the gap between the layers leads to weakening the Van-der Waal forces. The enlarged graphite host gallery upon initial Li-intercalation makes subsequent intercalation stages easier. The relative drop of voltage is more in graphite (0.45 V) compared to composite (0.24 V) in the low-capacity region (<50mAh g⁻¹), reflecting the experimental trend, where the voltage drop has been found more in the case of WG compared to WG@GNF. To find out the underlying reason for such drastic voltage drop in graphite by analyzing the binding behaviour of Li atom into the graphite and composite. To quantify the results, we have calculated the binding energy of a single Li-atom into the graphite as well as the composite layer. As shown in the relaxed structure of Figure 5c, the binding energy of Li-atom are 0.80 and -3.32 eV into the graphite and composite structure, respectively. The strong binding nature is attributed to the bonding between Li and O-atoms, which is reflected in the charge density difference plot also, as shown in the bottom panel of Figure 5c, which clearly shows that the charge accumulation in the graphene layers of graphite structure is more compared to that of the composite structure. Concomitantly the charge depletion is more at the Li-center, thus indicating that the charge depletion in the Li atom is compensated by the O-atom, as evidenced from the accumulated charge density at the O-center. Such charge compensation by O-atoms retains the trend in case of higher Li concentration, as shown in Supporting Information Figure S8a. Since the charge transfer is facilitated by O-atoms and the therefore, the follow-up opening of the adjacent gallery becomes thermodynamically more favourable in the case of composite structure compared to that of graphite structure. To probe this assumption, we have simulated the Li-intercalation in the adjacent layer to the stage-4' as has been shown in Supporting Information Figure S8b. The calculated average binding energy of 1 Li into the adjacent layer are -1.71 and -1.56 eV for composite and graphite systems, respectively. The corresponding CDD plot (bottom panel of Supporting Information Figure S8b) also reveals that
charge depletion around the Li atoms is significantly higher in composite graphite. Therefore, it is established from the binding energy and CDD plot of the second layer intercalation that the less charge density at the carbon atoms upon first layer intercalation facilitates the charge transfer between carbon atoms and Li-atoms, making the process thermodynamically favourable in the case of composite, which results in a decrease of the voltage drop in composite structure compared to graphite structure.

In this context, we have looked into the electronic behaviour of the WG and WG@GNF composite systems to check their nature of electronic conductivity. Supporting Information Figure S9 shows that both WG and WG@GNF systems possess a continuous density of states (DOS) at the Fermi level. However, the composite system shows more intense DOS at the Fermi level, thus can attribute the possibility of increased conductivity and a monotonic discharge curve in composite structure compared to graphite, thus supporting the voltage profile trends.
Figure 5. (a) Optimized geometries of WG and WG@GNF composite systems along with the different stages. (b) Voltage profile diagram for the different stages of Li intercalation. (c) Optimized structure with one Li intercalation in graphite and composite structures (upper panel) and the corresponding CDD plot (bottom panel).
Figure 6. (a) Galvanostatic charge-discharge voltage profile of WG@GNF at 0.5 C (1C = 372 mAh g$^{-1}$) in the voltage range of 0.01-3V, (b) the histogram quantifying the capacity contribution from surface adsorption $> 0.2$V and intercalation $< 0.2$V at 0.5 C, (c) comparison of cycling stability plot between WG@GNF and WG at 0.5 C (d) C-rate performance, (e) charge-discharge voltage
profile of WG@GNF at various current densities (inset: stagewise Li-ion intercalation at lower potential) and (f) comparison of cycling stability plot between WG@GNF and WG at a higher current density of 500 mA g\(^{-1}\).

WG@GNF is exposed to charge-discharge cycling at a higher current density of 0.5 C rate after five formation cycles at 0.1 C. Figure 6a shows that WG@GNF delivers an enhanced initial stable discharge and charge capacity of 400 mAh g\(^{-1}\) and 392 mAh g\(^{-1}\). Figure 6b represents the histogram for the WG@GNF electrode for the 1\(^{st}\), 2\(^{nd}\), 150\(^{th}\) and 300\(^{th}\) cycles at 0.5 C-rate, with a significant contribution of absorption capacity for WG@GNF, which is almost negligible for WG. WG shows relatively lower discharge and charge capacities of 310 mAh g\(^{-1}\) and 302 mAh g\(^{-1}\) (Figure 6c). At the end of the 300\(^{th}\) cycle, WG@GNF and WG exhibit discharge capacities of 354 mAh g\(^{-1}\) and 290 mAh g\(^{-1}\), respectively. WG@GNF shows superior cycling stability with an average discharge capacity of 368 mAh g\(^{-1}\) with 99% coulombic efficiency, which is 1.2 times higher than WG at a 0.5 C rate, as represented in Figure 6c.

The rate capability studies for WG@GNF and WG are carried out in various current densities (five cycles each) ranging from 50 mA g\(^{-1}\) to 5 A g\(^{-1}\). When the current densities are varied from 50 mA g\(^{-1}\) to 100 mA g\(^{-1}\), 200 mA g\(^{-1}\), 500 mA g\(^{-1}\), 1 A g\(^{-1}\), 2 A g\(^{-1}\), and 5 A g\(^{-1}\), WG@GNF shows the average specific capacities of 530, 490, 395, 293, 161 and 92 mAh g\(^{-1}\), respectively (Figure 6d). Figure 6e represents the corresponding charge-discharge voltage profile with an inset figure indicating stepwise Li\(^{+}\) intercalation into the graphite sheets. In comparison, Supporting Information Figure S10 shows that WG delivers negligible capacities at such high current densities. At a current density of 1 A g\(^{-1}\), the capacity enhancement in WG@GNF is 5.8 times compared to WG. Based on this observation, we have carried out long-term cycling at 500 mA g\(^{-1}\) over 1000 cycles (after 10 formation cycles). Figure 6e represents that WG@GNF exhibit
significantly enhanced initial discharge and charge capacities of 380 and 375 mAh g\(^{-1}\). At the 1000\(^{th}\) cycle, the capacity becomes 235 mAh g\(^{-1}\) with 62 % capacity retention with respect to initial stable capacity. In comparison, WG delivers an average discharge capacity of 156 mA g\(^{-1}\) and 58 % capacity retention under similar conditions.

Supporting Information Table S3 represents the present work compared to the reported literature on graphite recycling, indicating graphite recovery technique, post-purification strategies for enhancing electrochemical activity (including acid washing, catalytic activity, and carbon coating), initial stable discharge capacity, current density, cycle-life, and capacity retention.\(^{4,25–29,29–31,55,56}\) It is observed that WG@GNF delivers better capacity value in both a low rate of 0.5C and a high rate of 500 mA g\(^{-1}\) with good cycling stability over 1000 charge-discharge cycles, which is superior or

Further, to investigate Li\(^{+}\) kinetics, electrochemical impedance spectroscopy (EIS) is measured for WG@GNF after 1\(^{st}\) cycle (Figure 7a) and the 100\(^{th}\) cycle (Figure 7b), respectively, in the frequency range of 1 MHz to 0.01 Hz. The plots after 1\(^{st}\) cycle consist of a semicircle in the high-frequency region, indicating charge transfer resistance (R\(_{CT}\)), and a linear sloping tail at the low-frequency region, representing Li\(^{+}\) diffusion into the bulk of the matrix. However, two depressed semicircles appear after cycling. The first semicircle in high frequency is attributed to SEI, and the second one is the charge transfer resistance. R\(_{CT}\) values for WG@GNF are increased from 20 \(\Omega\) cm\(^2\) in 1\(^{st}\) cycle to 67 \(\Omega\) cm\(^2\) in the 1000\(^{th}\) cycle. Li\(^{+}\) diffusivity is further elucidated from the EIS spectra at low-frequency regions.\(^{35,36,58}\) The Warburg factor (\(\sigma\)) of WG@GNF is evaluated from the slope of the plot between Z’ and the reciprocal of the square root of frequency (\(\omega^{-1/2}\)). Figure 7c shows a linear relationship after the 1\(^{st}\) and 1000\(^{th}\) cycle, and the corresponding slopes (\(\sigma\)) are calculated. It is observed that Li-ion diffusivity at the end of the 1000\(^{th}\) cycle (\(D_{1000}\))
of the WG@GNF electrode becomes almost six times compared to the 1st cycle. It might be due to the reorientation of graphene sheets on long-term cycling that generates more space for Li$^+$ transportation during the lithiation and delithiation process in the WG@GNF electrode. The diffusion coefficient (D) value before and after cycling is compared as follows.

$$D_{1000} = \left( \frac{\sigma_1}{\sigma_{1000}} \right)^2 D_1$$

![Figure 7. Nyquist plot of WG@GNF electrode (a) after 1st cycle and (b) after the 1000th cycle, and (c) the corresponding linear fitting between $Z'$ and $\omega^{-1/2}$ in the low-frequency region after 1st and 1000th cycles.]

The above electrochemical studies reveal that the specific capacity of recycled graphite can be enhanced by 1.2-2 times by using recycled graphene as an additive. The voltage profile (Figure 4c) demonstrates that the parabolic slopping voltage curve > 2V incorporates the extra achievable capacities in WG@GNF, which is almost negligible in WG, as observed from the histogram analysis in Figure 4d and Figure 6b. The advanced mechanisms involved in higher charge storage phenomena, in addition to Li$^+$ intercalation into the graphite layers, are attributed to (i) more Li-ion accommodation on both sides and edges of graphite sheets to form LiC$_x$, (ii) chemi-adsorption
of Li$^+$ to the oxygen functionalities as observed from FTIR (Figure 2d) and XPS (Figure 2e) studies and (iii) nanopore filling of Li$^+$.\textsuperscript{59,60} Moreover, the trapped graphite particles in WG@GNF (as observed from SEM in Figure 1c) might hinder the agglomeration of wrinkled graphite flakes and provides mechanical stability over long-term cycling. Scheme 2 represents the pictorial diagram of different Li$^+$ storage mechanisms in WG@GNF compared to recycled GNF and WG.

Scheme 2. Pictorial representation of different Li$^+$ storage mechanisms of recycled graphite, GNF, and WG@GNF.

To understand the morphological variations of the WG@GNF anode on continuous cycling, FESEM analysis is carried out after 1000 charge-discharge cycles, as shown in Supporting Information Figure S11. The thickness of the anode coating before the cycling electrode is expanded from 20-25 $\mu$m (Supporting Information Figure S11a) to 50-55 $\mu$m (Supporting
Information Figure S11b) for the after-cycled electrode. Supporting Information Figure S11c-d indicates the appearance of SEI surface film-like secondary particles and deposition of new particles, which are expected to comprise inorganic Li salts (e.g., Li$_2$O, Li$_2$CO$_3$, Li alkyl carbonates, LiF, etc.) and organic oligomers (ROCOOLi and ROLi, where R is alkyl groups of low molecular weight) that are formed via reductive decomposition of the electrolyte. Further, to check the practical feasibility of the WG@GNF anode, full cells are fabricated with commercial NMC 811 and LFP cathode. The cathode and anode weight ratio is maintained at ~2.8:1. The capacity vs. voltage profile for NMC 811 and LFP cathode at 0.1 C rate shows the half-cells deliver an average capacity of 180 mAh g$^{-1}$ and 160 mAh g$^{-1}$, respectively, as shown in (Supporting Information Figure S12a and S12b). The full cells fabricated with NMC811 // WG@GNF and LFP // WG@GNF deliver an initial discharge capacity of 120 mAh g$^{-1}$ and 140 mAh g$^{-1}$ at C/3 rate in the voltage window of 2.8-4.3 V and 2.8-3.5 V, respectively, and the cells show quite stable electrochemical performance (Figure 8). This study manifests that the electrochemical activity of spent graphite anode can be revitalized, and recycled WG@GNF is a promising anode material for high-performance LIBs.
Figure 8. Full cell analysis of (a) charge-discharge voltage profile and (b) discharge capacity vs. cycle number for WG@GNF anode and commercial NMC-811 cathode in the voltage window of 2.8-4.3V, (c) charge-discharge voltage profile and (d) discharge capacity vs. cycle number for WG@GNF anode and commercial LFP cathode in the voltage window of 2.8-3.5V.

Conclusions

Recovery of value-added electrode materials from spent LIBs such as Li, transition metals (Co, Ni, Mn) and battery-grade graphite has been maneuvered in recent years for economic incentives and resource sustainability. The advantage of the retention of the bulk structural integrity of the cycled graphite has garnered much interest for second-life Li-ion storage. Herein, anode graphite material is recovered from spent LIBs by water leaching followed by post-purification via inert-atmosphere calcination to enhance the degree of graphitization. Graphene nanoflakes (GNF) are prepared from the recovered water-washed graphite (WG) by Hummer’s method, followed by thermal reduction. Electrochemistry depicts that pure GNF anode experiences a very high irreversible capacity loss (~50%) during initial cycles due to irreversible Li\(^+\) trapping in surface heteroatom functionalities, defect sites, and nanopore filling. Despite being a high-capacity anode material, this causes a big hurdle for commercializing pure graphene systems. However, the high charge-storage capability of GNF can be utilized, and the site-limited diffusivity of recycled graphite anode can be enhanced by amalgamating an optimized amount of GNF additive (i.e., 20 wt. %) to the recycled WG matrix with a proper balancing between high specific capacity and long-term cycling stability. The extra achievable capacity in WG@GNF is originating from more Li-ion intercalation into larger d-spacing (as observed in the XRD plot) and chemisorption to the controlled surface functionalities (as observed in FTIR, XPS and EDX analysis). A synergistic phenomenon comprised of Li-ion adsorption (slopy region capacity) and intercalation (plateau
region capacity) in WG@GNF resulted in an enhanced average capacity of ~368 mAh g\(^{-1}\) at 0.5C over 300 cycles and ~320 mAh g\(^{-1}\) at a higher current density of 500 mA g\(^{-1}\) over 1000 cycles, which is almost 1.2-2 times in comparison to recovered WG (~295 mAh g\(^{-1}\) at 0.5C and ~156 mAh g\(^{-1}\) at 500 mA g\(^{-1}\)). The electrochemistry results are further supported by DFT calculations considering the WG@GNF and WG models. The DFT results demonstrate that the strong Li adsorption with oxygen functionalized sites plays a key role in the low voltage drop across the slopy capacity region. Additionally, it has been established that the thermodynamic feasibility of the Li-ion intercalation process is attributed to the charge density of the layers of the graphite. Besides, the unique SEM morphology of entrapping spherical graphite particles among wrinkled graphite flakes reduces the crumbling of graphene flakes and provides structural stability over long-term cycling. Impedance studies display that the WG@GNF anode facilitates almost 6 times more diffusivity at the end of the 1000\(^{th}\) cycle. To showcase the practical feasibility of the WG@GNF anode, the full cell is fabricated with commercial LFP and NMC-811 cathode that demonstrates optimum electrochemical performance. It is believed that WG@GNF is a potentially feasible anode material for upscaling applications. This strategy paves a sustainable and economically viable avenue to improvise the electrochemical compatibility of recycled graphite anode from spent Li-ion batteries.

**Associated contents**

Supporting Information

Reported graphene-carbon composite and electrochemistry in comparison to our studies; computational models for WG and WG@GNF; EDS of recovered, purified graphite and WG@GNF, TEM images of WG and GNF; XRD of GNF; simulated XRD; optimization of GNF additive in capacity vs. voltage profile and the comparative study of irreversible capacity; CV of
GNF; CDD plot; density of states; C-rate for WG; FESEM image for before and after cycling WG@GNF electrode; a comparison table between the reported literature and the present study indicating anode recovery, post-purification strategy and their electrochemical performance; capacity vs. voltage profile for NMC 811 and LFP cathode.

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